

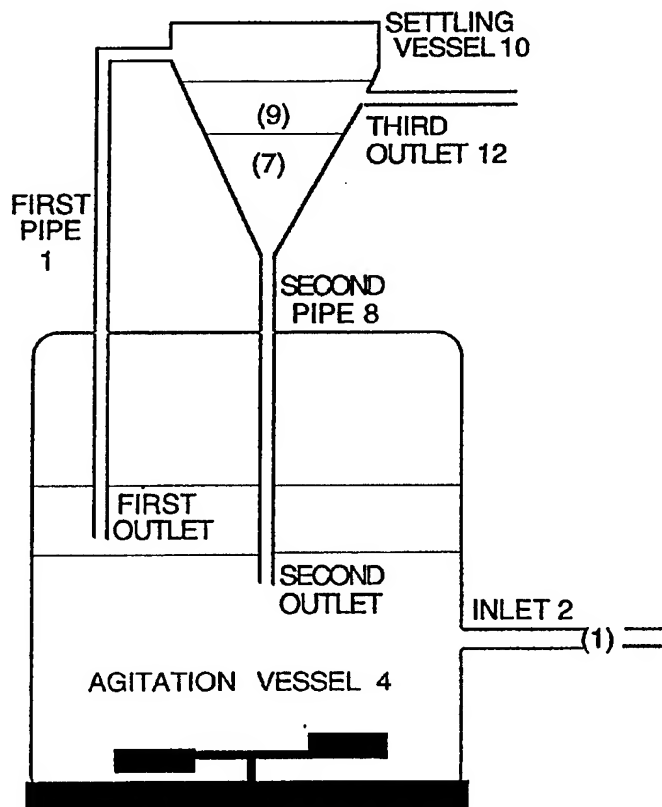


## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

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**(54) Title:** CONTINUOUS SETTLING APPARATUS**(57) Abstract**

An apparatus for continuously contacting and then separating particles or immiscible liquids from a liquid medium has an agitation vessel (4) with inlet (2). A settling vessel (10) is disposed above the agitation vessel (4) and connected to the agitation vessel (4) via a first pipe (1) and a second pipe (8). Liquid is drawn from the settling vessel (10) through a third outlet (12) when the lower ends of both the first pipe (1) and the second pipe (8) are covered by liquid. When enough liquid is withdrawn from the agitation vessel (4) through the settling vessel (10) to uncover the lower end of the first pipe (1), gas is drawn through the first pipe and liquid in the settling vessel (10) returns to the agitation vessel (4).



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**CONTINUOUS SETTLING APPARATUS**5           **Background of the Invention**

Since the development of the *in vitro* cultivation of cells the demand for large scale production of these cells and the products they express has increased. There is an increasing interest to use *in vitro* cultivated cells as recombinant hosts for the production of cellular products as potential diagnostic and therapeutic agents because for many of these agents, cell culture systems provide the only viable production source. These useful agents include monoclonal antibodies, human growth hormones, lymphokines, erythropoietin, blood clotting factors, and tissue plasminogen activators.

Cells, in particular mammalian, have the capability to synthesize these agents with the proper configuration, correct disulfide bonding, and arrays of sugar side chains which result in the desired activity of the naturally occurring agent. Therefore, many agents derived from cells are more likely to be efficacious and are less likely to be immunogenic in mammals if expressed by mammalian cells than if produced by bacterial or yeast fermentation.

Continuous suspension cell culture systems or perfusion systems offer distinct advantages over batch culture for large scale *in vivo* production of biopharmaceuticals. For example, in such systems, cells are constantly provided with fresh nutrients and depleted of toxic byproducts resulting in higher cell densities.

At such high cell densities, the requirements for serum decrease dramatically. For the purpose of downstream processing it is extremely important to minimize the level of serum

and thus reduce the major source of contaminant proteins such as albumin, transferrin, serum-derived immunoglobulin, proteases, protease inhibitors, etc., contained in the removed media.

5           In a state of continuous perfusion, products secreted by the cells which are vulnerable to biodegradation and aggregation at 37°C can be removed from the bioreactor and transported to a 4°C environment in readiness for subsequent  
10           purification. The rate of product removal from this labile cellular environment is in terms of only hours for perfusion systems as compared to many days and weeks for semi-batch systems respectively. This continuous harvesting process minimizes  
15           proteolytic degradation and aggregation processes.

          However, for most of these systems current methods of harvesting require filters to prevent the loss of the cells through the harvesting. Filters can become clogged causing the shut down of  
20           the system. A need exists to develop a more efficient method which allows the harvesting of the desired product without disruption. This need grows progressively more acute as biotechnology and pharmaceutical companies look to cut processing  
25           costs. Any elimination of problems which interfere with the continuous operation of these systems would increase their efficiency and subsequently reduce the cost of the biopharmaceutical agents.

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**Summary of the Invention**

This invention relates to an apparatus for suspending particles in a continuous flow of liquid. The apparatus comprises: 1) an agitation vessel, containing particles suspended in the liquid, wherein the density of each particle is greater than the liquid density; 2) a flow means for the continuous flow of liquid into the agitation vessel; 3) a first variable inlet/outlet means for allowing the periodic flow of a portion of the particle suspension from the agitation vessel to a settling vessel; 4) a second variable inlet/outlet means for allowing the free flow of a portion of the particle suspension between the agitation vessel and the settling vessel; 5) a settling vessel located above the agitation vessel which comprises: i) a body means for allowing the settling of the particles whereby the particles separate from a portion of the liquid; and ii) an outlet means for allowing the removal of liquid; and 6) a vacuum means for drawing a portion of the particle suspension into the settling vessel and for periodically removing a portion of the liquid out of the settling vessel, whereby a continuous flow of the liquid enters into the apparatus and a portion of the liquid periodically exits the apparatus wherein the liquid exiting the apparatus is particle free. In addition, the apparatus of the present invention is suitable for growing particles or for separating liquids of different densities.

The present invention further relates to an apparatus for releasing and collecting liquid containing liquid-soluble substances from particles. The apparatus comprises all of the elements of the apparatus explained above with the additional element of a collection means for the collection of the liquid containing the liquid-soluble substances. Furthermore, the apparatus of

the present invention is suitable for producing biological products released from cells and collecting the liquid containing the biological product.

5           The apparatus of the present invention allows for the continuous flow of new liquid or media to be added to a suspension of particles while allowing the removal of old liquid or media from the suspension; the removed liquid or media  
10           being free of the particles. The design of the present invention is such that there is no need for microfilters, hollow fibers, or any other type of filter device and, as such, the problems associated with these devices are avoided.

15           Brief Description of the Drawing

          Figure 1 is a schematic illustration of an embodiment of the present invention.

20           Figure 2 is a schematic illustration showing a cell culture apparatus with the preferred embodiment of the present invention.

25           Figure 2 is a graph showing the comparison of cells grown in a cell culture apparatus with the preferred embodiment of the present invention versus cells grown in a conventional batch type procedure.

30           Detailed Description of the Invention

          This invention is based upon the discovery that a continuous flow culture apparatus, which does not require filters, could be constructed  
35           using a modified inverted Erlenmeyer flask. The modified inverted Erlenmeyer flask, placed above and connected to a conventional cell culture vessel, provided a zone where microcarriers could settle while allowing for the removal of some of

the media without removing microcarriers. The apparatus provided for the continuous culturing of anchorage-dependent cells in fresh media while removing media containing proteins expressed by the cells.

While the specification concludes with claims particularly pointing out and distinctly claiming the subject matter regarded as forming the present invention, it is believed that the invention will be better understood from the following description in connection with Figure 1. Figure 1 is a schematic illustration of one embodiment of the present invention. Liquid (1) enters into agitation vessel 4 through inlet 2 and mixes with particles (3) contained in the agitation vessel. The particles and the liquid are mixed together for a time sufficient to suspend the particles in the liquid to produce particle suspension (5). As the new liquid enters agitation vessel 4 the level of the particle suspension rises to the bottoms of second inlet/outlets 8 and then first inlet/outlet 6. As a result of the level of particle suspension (5) reaching and contacting the bottom of the first inlet/outlet and the outward air flow created by a vacuum device connected to outlet 12, a negative air pressure (i.e., negative relative to the air pressure in the agitation vessel) develops in settling vessel 10. As the negative air pressure in the settling vessel increases, the suspension is drawn up into the inlet/outlets and into settling vessel 10. While in the non-agitated environment of the settling vessel, particles (3) begin to settle to the bottom of settling vessel 10, creating a strata of two zones. The lower zone contains concentrated particle suspension (7) and the upper zone contains particle-free liquid (9). As the negative air pressure continues to increase in the settling vessel the top level of the upper zone migrates to

outlet 12. Once the upper zone reaches outlet 12 the outward air pressure draws a portion of liquid (9) out of settling vessel 10. The loss of a portion of the liquid out of the settling vessel has the effect of lowering the level of the particle suspension (5) in the agitation vessel. Once the level in agitation vessel 4 drops below and loses contact with first inlet/outlet 6, the air pressure in settling vessel 10 is neutralized allowing the contents of the settling vessel (i.e., concentrated particle suspension (7) plus a portion of particle free liquid (9)) to empty back into the agitation vessel. This action of forcing the particles that temporarily collected in the settling vessel back into agitation vessel 4, prevents the loss of the particles through the outlet. The above explained cycle then repeats once the level of the particle suspension rises to the bottom and contacts the first variable inlet/outlet due to the accumulation of liquid that collects in agitation vessel 4 as a result of the flow of liquid entering the agitation vessel.

The term "particles" is intended to include any synthetic or biological substance or any substance with a synthetic and biological component. For example, the particles of the present invention include biological cells such as hybridoma cells. In the alternative the particles have a synthetic and biological component, such as anchorage-dependent cells attached to polyacrylamide microcarriers or polymer encapsulated cells.

Any liquid can be used in the apparatus of the present invention. Suitable liquids include aqueous solutions such as nutrient medium, for example Dulbecco's Modified Eagles Medium (Gibco, Grand Island, NY). Particle suspension refers to the random dispersion of particles in a liquid, the dispersion of the particles being caused by an



agitation device, such as a propeller. It should be noted that in order for the apparatus of the present invention to function properly each particle needs to have a density greater than the liquid density, i.e., have sufficient density to be able to settle, due to gravitational force, when in a non-agitated environment.

Emulsion refers to the random dispersion of one liquid in another. It should be noted that the liquids need to have different densities in order to subsequently effect separation.

Any vessel mentioned above or herein, must be a container with inner containment walls constructed of an inert material, i.e., a material that will not leach or react when in contact with the particles or liquid used in the present invention. In a one embodiment, vessels with inner containment walls constructed of stainless steel are preferred.

The agitation vessel of the present invention encompasses any vessel equipped with an agitation device. Suitable agitation devices include mechanical means, hydrodynamic means, or ultrasonic means using a conventional bath or probe sonication device. Mechanical means include axial-flow impeller-type mixers such as marine-type mixing propeller or pitched-blade turbine, or radial-flow impellers such as curved-blade turbine or flat-blade turbine. The main criteria for any agitation device used in the apparatus of the present invention is that the portion of the device that comes in contact with the particles should not cause their fracturing or shearing or such action should be kept to a minimum.

The term "flow means" is intended to describe any device capable of causing the continuous flow of liquid into the agitation vessel. The term "vacuum means" is intended to describe any device capable of creating negative

air pressure (i.e., air pressure below that which is present in the agitation vessel) in a closed vessel and capable of removing liquid from a vessel. In both cases, suitable devices include peristaltic-type, diaphragm-type, gear-type, piston-type and rotary-lobe type pumps. The main criteria for any pump used for either purpose in the apparatus of the present invention is that the portion of the pump that comes in contact with the liquid should be inert and not react with the liquid by changing or adding to the its composition.

The term "second variable inlet/outlet means" is intended to mean any device which allows for liquid to flow freely, in either direction, between two vessels. Suitable devices include any pipe, tube, hose or any other cylinder with an inner containment wall constructed of inert material such as stainless steel.

The term "first variable inlet/outlet" is intended to mean any device which allows the flow of liquid from the agitation vessel to the settling vessel, as described above, but only in a periodic fashion. This can be accomplished by having the first variable inlet/outlet not extend as far into the agitation vessel as the second variable inlet/outlet means, as shown in Figure 1. The length differential allows for the negative air pressure to return to the pressure in the agitation vessel when the liquid level in the agitation level is no longer in contact with the first variable inlet/outlet means. The process of periodically allowing negative air pressure to develop in the settling vessel is explained in detail above (see Figure 1).

In addition, it should be noted that in circumstances where the liquid used in the apparatus of the present invention produces foam, as in the case with some nutrient media, a device

(or anti-foaming agent) to remove the foam from the apparatus or to prevent the foam from entering the first variable inlet/outlet means needs to be used. Foam that forms in the agitation vessel can be drawn up into the settling vessel preventing the proper function of the apparatus. In a preferred embodiment, the apparatus of the present invention the first variable inlet/outlet means includes a collar which prevents foam from entering the first variable inlet/outlet means. The collar can consist of a bell shaped cylinder, with holes drilled at the top, which attaches and extends beyond the bottom of a pipe used as a first variable inlet/outlet means. Suitable collars are constructed of inert material, preferably stainless steel.

The term "settling vessel" refers to any vessel which provides a non-agitated environment apart from the agitation vessel. The settling vessel of the present invention needs to have an inert inner containment wall, as explained above, and a shape which does not prevent particles from returning to the agitation vessel. For example, a suitable settling vessel would be constructed with inner walls of stainless steel and have a conical shape. In a preferred embodiment, the settling vessel is a cylinder with a conical shaped bottom portion and a closed top (see Figure 1). It should be noted that in order for the settling vessel of the present invention to function properly it needs to be located above the agitation vessel. In addition, the settling vessel has at least one port connected to the second variable inlet/outlet means, at least one port connected to the first variable inlet/outlet means and at least one port connected to the outlet means. In order for any settling vessel to function properly in the apparatus of the present invention any port in the settling vessel that is connected to the first

variable inlet/outlet means should be located above any port in the settling vessel connected to the outlet (in the settling vessel), and any port in the settling vessel connected to the second  
5 variable inlet/outlet means should be located below the port in the settling vessel connected to the outlet.

The term "liquid-soluble substances" refers to any substance that is soluble in the particular  
10 liquid used in the apparatus of the present invention and is generated by the particles. The term "biological products" refers to any substance produced by a biological organism such as cell expressed protein.

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The invention will be further illustrated by the following non-limiting Exemplification:

#### **EXEMPLIFICATION**

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##### **Materials and Methods:**

A standard 125 ml Erlenmeyer flask was modified by attaching a    inch diameter glass tubing to the side of the flask just below the top of the flask as inverted (see the Figures). In  
25 addition, the neck was extended and narrowed to a    inch diameter.

Cytodex III microcarriers were purchased from Pharmacia, Piscataway, NJ. The microcarriers are spherical objects made of dextran with a  
30 diameter of approximately 200  $\mu\text{m}$ . The microcarriers were coated with a layer of porcine collagen to promote cell attachment.

Anchorage-dependent mammalian cells were grown in nutrient medium.

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A glass 2 liter vessel purchased from Bellco Glass, Inc. (Vineland NJ) was used as the agitation vessel. The vessel was equipped with a teflon paddle and magnetic stir bar and connected to mixed gas ( $\text{O}_2$ ,  $\text{CO}_2$ ,  $\text{N}_2$ ) to maintain the pH and dissolved

oxygen level of the nutrient media. The movement of the magnetic stir bar was controlled by a magnetic stir bar plate positioned underneath the bottom of the agitation vessel (purchased from Bellco Glass).

A 5 liter glass vessel purchased from Bellco Glass was used as a media supply vessel.

A 10 liter polycarbonate carboy was used as a harvest vessel.

Pumps used were peristaltic-type pumps purchased from Cole-Parmer Instrument Co. (Chicago, IL).

#### **Continuous Cell Culture Apparatus** (see Figure 2):

One liter of media containing microcarriers and anchorage dependent cells were placed into the agitation vessel.

The media supply vessel was connected to the agitation vessel by silicone tubing. A peristaltic pump was positioned between these two vessels to pump fresh nutrient medium into the agitation vessel.

The settling vessel, constructed as explained above, was positioned above the agitation vessel. The pipe extending from the side of the settling vessel was connected to a    inch stainless steel tube which was then inserted into the agitation vessel. In addition, a bell shaped cylinder with holes drilled through the top (i.e., collar) was attached and extended beyond this    inch pipe. Another    inch pipe was connected to the mouth of the inverted Erlenmeyer flask (i.e., settling vessel) and inserted into the agitation vessel running parallel to the other    pipe and extending further into the agitation vessel than both said    inch pipe and collar attachment.

The outlet of the settling vessel was connected via silicone tubing to the harvest

vessel. A peristaltic pump was positioned between the settling vessel and the harvest vessel to create a vacuum in the settling vessel to draw the microcarrier suspension into the settling vessel and for the removal of media.

#### **Operation of Continuous Cell Culture Apparatus:**

The agitation was set at 30 rpm to maintain the microcarriers in suspension.

Dissolved oxygen was maintained between 10 and 20 mm Hg by adjusting the percent oxygen in the overlay.

The pump positioned between the media supply vessel and the agitation vessel was set at one liter per day rate.

The pump positioned between the settling vessel and the harvest vessel was set at slightly faster than one liter per day rate.

The operation of the apparatus was maintained for 21 days and the agitation of the microcarriers was not suspended for the duration.

#### **Comparison with Batch-Type Procedure:**

Cells grown as described above were compared with cells grown by a conventional batch type method (fedbatch) for the same time frame.

The apparatus used for the batch method was constructed similarly to the agitation vessel described above, i.e., a glass 2 liter vessel equipped with a teflon paddle and magnetic stir bar and connected to mixed gas. As in the above described apparatus the magnetic stir bar was controlled by a magnetic stir bar plate, however, the batch apparatus was not connected to an inverted Erlenmeyer flask (i.e., settling vessel) as explained above.

The batch cells were maintained by replacing approximately 80% of the nutrient media every 24 hours. The media was replaced by stopping the

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agitation caused by the magnetic stir bar, allowing the microcarrier attached cells to settle, aspirating off and replacing 80% of the nutrient media with fresh media and starting the agitation of the microcarriers again.

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Figure 3 is a graph that compares the cells grown in the apparatus explained in detail above and the cells grown by the batch method. Because of the physical setup of the continuous settling apparatus there was no port available on the agitation vessel for gas entry therefore there was an oxygen limitation which limited cell number. There problem is easily rectified by modifying the agitation vessel by creating a port for gas entry.

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**CLAIMS**

1. A continuous settling apparatus comprising:
  - a. an agitation vessel comprising:
    - i. a hollow body;
    - ii. an agitation device capable of maintaining particles suspended in a liquid; and
    - iii. a flow means for the continuous flow of the liquid into the agitation vessel;
    - iv. a first and a second pipe and outlet for allowing the free flow of a portion of the particle suspension from and to the settling vessel.

whereby a continuous flow of the liquid enters into the agitation vessel and a portion of the liquid periodically reaches the third outlet and exits the settling vessel wherein the liquid exiting is particle free.
2. The apparatus of Claim 1 wherein the settling vessel has a conical shape.
3. An apparatus for separating liquids of different densities, comprising:
  - a. an agitation vessel, comprising:
    - i. a hollow body;
    - ii. an agitation device capable of producing an emulsion consisting of two liquids, a first liquid with a density greater than a second liquid;
    - iii. a flow means for the continuous flow of the second liquid into the agitation vessel; and



- 5                   iv.    a first and a second pipe and  
                    outlet for allowing the free flow  
                    of a portion of the emulsion from  
                    and to the agitation vessel  
                    wherein the second pipe is longer  
                    than the first pipe; and
- 10           b.    a settling vessel located above the  
                  emulsion level in the agitation vessel  
                  and in liquid communication with the  
                  agitation vessel, comprising:
- 15               i.    a hollow body wherein the shape of  
                    the hollow body allows for the  
                    settling of the first liquid from  
                    the second liquid, thereby  
                    separating the liquids;
- 20               ii.   a third outlet for allowing the  
                    removal of the second liquid;
- 25               iii. a vacuum means connected to the  
                    third outlet for creating a vacuum  
                    in the settling vessel sufficient  
                    to draw a portion of the emulsion  
                    into the settling vessel from the  
                    agitation vessel and for removing  
                    the second liquid out of the  
                    settling vessel when it reaches  
                    the third outlet; and
- 30               iv.   a first and second inlet connected  
                    to the first and second pipes,  
                    respectively, for allowing the  
                    free flow of a portion of the  
                    particle suspension from and to  
                    the settling vessel,
- 35               whereby a continuous flow of the second  
                  liquid enters into the agitation vessel and  
                  the second liquid periodically exits the  
                  settling vessel when the level of the second  
                  liquid reaches the third outlet wherein the  
                  second liquid is free of the first liquid.

4. The apparatus of Claim 3 wherein the settling vessel has a conical shape.
- 5
5. An apparatus for growing cells adhered to particles in a continuous-flow liquid media culture, comprising:
- 10 a. an agitation vessel, comprising:
- i. a hollow body;
- 10 ii. an agitation device capable of maintaining the particles suspended in media;
- 15 iii. a flow means for the continuous flow of media into the agitation vessel;
- 20 iv. a first and a second pipe and outlet for allowing the free flow of a portion of the particle suspension from and to the agitation vessel wherein the second pipe is longer than the first pipe; and
- 25 b. a settling vessel located above the liquid level in the agitation vessel and in liquid communication with the agitation vessel, comprising:
- 30 i. a hollow body wherein the shape of the hollow body allows for the settling of the particles from a portion of the media;
- 35 ii. a third outlet for allowing the removal of media;
- iii. a vacuum means for creating a vacuum sufficient to draw a portion of the particle suspension into the settling vessel from the agitation vessel and for removing the media when the media level

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reaches the third outlet; and

- iv. a first and a second inlet connected to the first and second pipes, respectively, for allowing the free flow of a portion of the particle suspension from and to the settling vessel,

whereby a continuous flow of the media enters into the agitation vessel and a portion of the media periodically exits the settling vessel when the media level reaches the third outlet wherein the media exiting is particle free.

6. The apparatus of Claim 5 wherein the settling vessel has a conical shape.

7. An apparatus for releasing liquid-soluble substances from particles and collecting liquid containing the liquid-soluble substances, comprising:
- a. an agitation vessel, comprising;
- i. a hollow body;
- ii. an agitation device capable of maintaining particles suspended in liquid;
- iii. a flow means for the continuous flow of the liquid into the agitation vessel; and
- iv. a first and a second pipe and outlet for allowing the free flow of a portion of the particle suspension from and to the agitation vessel wherein the second pipe is longer than the first pipe; and

- 5                   b.    a settling vessel located above the  
                  liquid level in the agitation vessel  
                  and in liquid communication with the  
                  agitation vessel, comprising:
- 10                   i.    a hollow body wherein the shape of  
                  the hollow body allows for the  
                  settling of the particles form a  
                  portion of the liquid, whereby the  
                  separated liquid contains liquid-  
                  soluble substances released from  
                  the particles;
- 15                   ii.   a third outlet for allowing the  
                  removal of a portion of the  
                  separated liquid;
- 20                   iii. a vacuum means connected to the  
                  third outlet for creating a vacuum  
                  in the settling vessel sufficient  
                  to draw a portion of the particle  
                  suspension into the settling  
                  vessel from the agitation vessel  
                  and for removing a portion of the  
                  separated liquid out of the  
                  settling vessel when the liquid  
25                   reaches the third outlet; and
- 30                   iv.   a first and a second inlet  
                  connected to the first and second  
                  pipes, respectively, for allowing  
                  the free flow of a portion of the  
                  particle suspension from and to  
                  the settling vessel; and
- 35                   8.    The apparatus of Claim 7 wherein the  
                  settling vessel has a conical shape.
9.    An apparatus for producing and collecting  
                  biological products released from cells  
                  attached to particles, comprising:

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- a. an agitation vessel, comprising:
    - i. a hollow body;
    - ii. an agitation device capable maintaining particles suspended in a media;
    - iii. a flow means for the continuous flow of media into the agitation vessel; and
    - iv. a first and a second pip and outlet for allowing the free flow of a portion of the particle suspension from and to the agitation vessel wherein the second pipe is longer than the first pipe; and
  - b. a settling vessel located above the liquid level in the agitation vessel and in liquid communication with the agitation vessel, comprising:
    - i. a hollow body wherein the shape of the hollow body allows for the settling of the particles from a portion of the media, whereby the separated media contains biological product released from particles;
    - ii. a third outlet for allowing the removal of a portion of the separated media;
    - iii. a vacuum means connected to the third outlet for creating a vacuum sufficient to draw a portion of the particle suspension into the settling vessel from the agitation vessel and for removing the separated media out of the settling vessel when it reaches the third outlet; and
    - iv. a first and a second inlet

- connected to the first and second pipes, respectively, for allowing the free flow of a portion of the particle suspension from and to the settling vessel; and
- 5 c. a collection vessel, comprising:
- i. a hollow body; and
  - ii. an inlet for allowing the collection of the separated media
- 10 in the collection vessel,
- whereby a continuous flow of the media enters into the agitation vessel and the separated media periodically reaches the third outlet and exits the settling vessel
- 15 and the separated media is collected in the collection vessel wherein the collected separated media contains biological product released from the cells attached to the particles and is particle free.
- 20
10. The apparatus of Claim 9 wherein the settling vessel has a conical shape.
11. A continuous settling apparatus, comprising:
- 25 a. an agitation vessel, comprising:
- i. a hollow body; and
  - ii. an agitation device;
- b. a settling vessel located above the liquid level in the agitation vessel,
- 30 comprising:
- i. a conical shaped body wherein the body is aligned vertically, with the narrow portion being the bottom;
  - 35 ii. at least one pipe exiting a first port on the side portion of the body of the settling vessel, being connected to a second port on the body of the agitation vessel and

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the pipe extending into the  
agitation vessel;

- 5                   iii. at least one pipe exiting a third  
port on the bottom portion of the  
body, being connected to a fourth  
port on the body of the agitation  
vessel and extending further into  
the agitation vessel than the pipe  
connected to the first and second  
10                   port; and
- iv. at least one pipe exiting a fifth  
port on the side portion of the  
body, the fifth port located below  
the first port and being connected  
15                   to a vacuum means.

12.           The apparatus of Claim 11 wherein the pipe  
connected to the first and second port has a  
bell-shaped collar attached to the end of  
20           the portion of the pipe that extends into  
the agitation vessel.

13.           An apparatus for growing cells attached to  
particles, comprising:
- 25           a. an agitation vessel, comprising;
- i. a hollow body; and
- ii. an agitation device; and
- b. a settling vessel located above the  
liquid level in the agitation vessel,  
30           comprising:
- i. a conical shaped body wherein the  
body is aligned vertically, with  
the narrow portion being the  
bottom;
- 35           ii. at least one pipe exiting a first  
port on the side portion of the  
body of the settling vessel being  
connected to a second port on the  
body of the agitation vessel and

extending into the agitation vessel;

- 5                   iii. at least one pipe exiting a third port on the bottom portion of the body of the settling vessel, being connected to a fourth port and extending further into the agitation vessel than the pipe connected to the first and second
- 10                   port; and
- iv. at least one pipe exiting a fifth port on the side portion of the body, the fifth port located below the first port and being connected
- 15                   to a vacuum means.

14.       The apparatus of Claim 13 wherein the pipe connected to the first and second port has a bell-shaped collar attached to the end of

20       the portion of the pipe that extends into the agitation vessel.

15.       An apparatus for growing cells in a continuous-flow liquid media culture, comprising:
- 25       a. an agitation vessel, comprising:
- i. a hollow body;
- ii. an agitation device capable of maintaining the cells suspended in
- 30       media;
- iii. a flow means for the continuous flow of media into the agitation vessel;
- iv. a first and second pipe and outlet
- 35       for allowing the free flow of a portion of the cell suspension from and to the agitation vessel wherein the second pipe is longer than the first pipe; and



- b. a settling vessel located above the liquid level in the agitation vessel and in liquid communication with the agitation vessel, comprising:
- 5 i. a hollow body wherein the shape of the hollow body allows for the settling of the cells from a portion of the media; and
- 10 ii. a third outlet for allowing the removal of media;
- 15 iii. a vacuum means connected to the third outlet for creating a vacuum in the settling vessel sufficient to draw a portion of the cell suspension into the settling vessel and for removing the media when the media reaches the third outlet; and
- 20 iv. a first and a second inlet connected to the first and second pipes, respectively, for allowing the free flow of a portion of the cell suspension from and to the settling vessel,
- 25 whereby a continuous flow of the media enters into the agitation vessel and a portion of the media periodically exits the settling vessel when the media reaches the third outlet wherein the media exiting the settling
- 30 vessel is cell free.

16. An apparatus for growing cells in liquid media, comprising:
- 35 a. an agitation vessel, comprising;
- i. a hollow body; and
- ii. an agitation device; and
- b. a settling vessel located above the liquid level in the agitation vessel,

comprising:

- i. a conical shaped body wherein the body is aligned vertically, with the narrow portion being the bottom;
- ii. at least one pipe exiting a first port on the side portion of the body of the settling vessel being connected to a second port on the body of the agitation vessel and extending into the agitation vessel;
- iii. at least one pipe exiting a third port on the bottom portion of the body of the settling vessel, being connected to a fourth port and extending further into the agitation vessel than the pipe connected to the first and second port; and
- iv. at least one pipe exiting a fifth port on the side portion of the body, the fifth port located below the first port and being connected to a vacuum means.

FIGURE 1

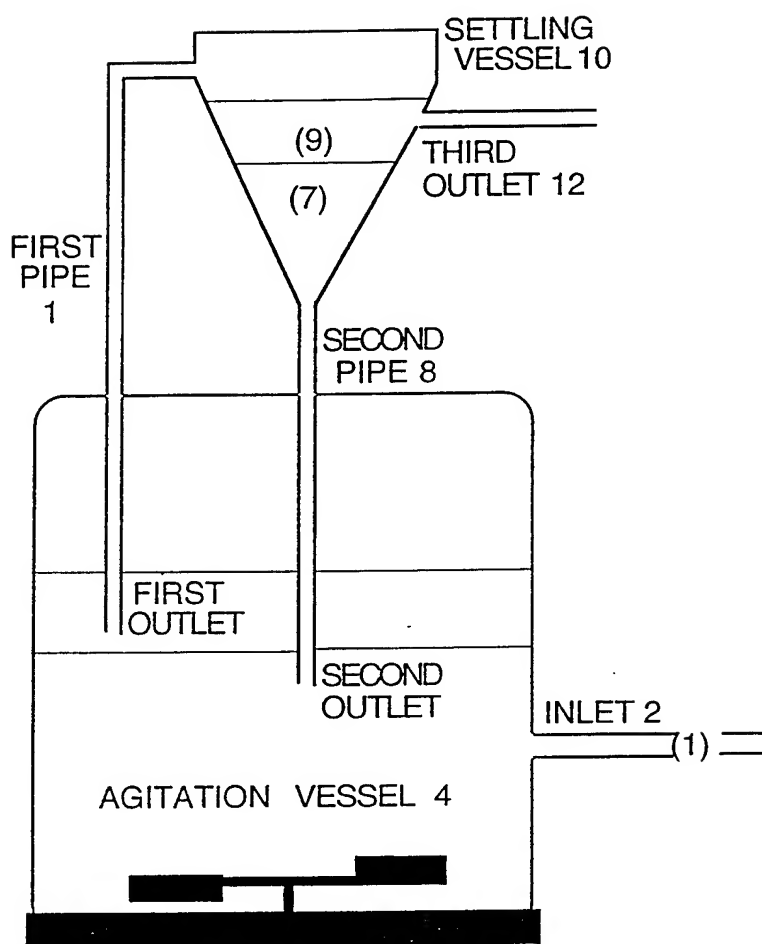


Figure 2

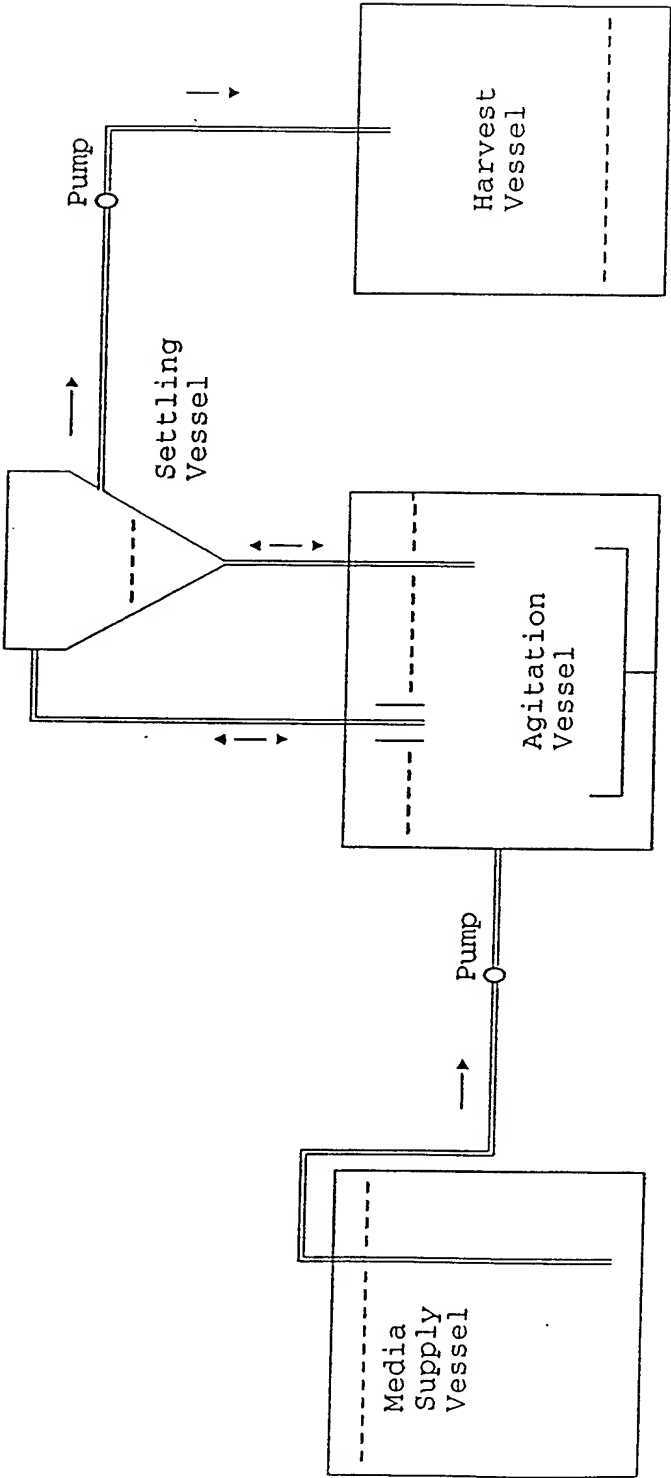
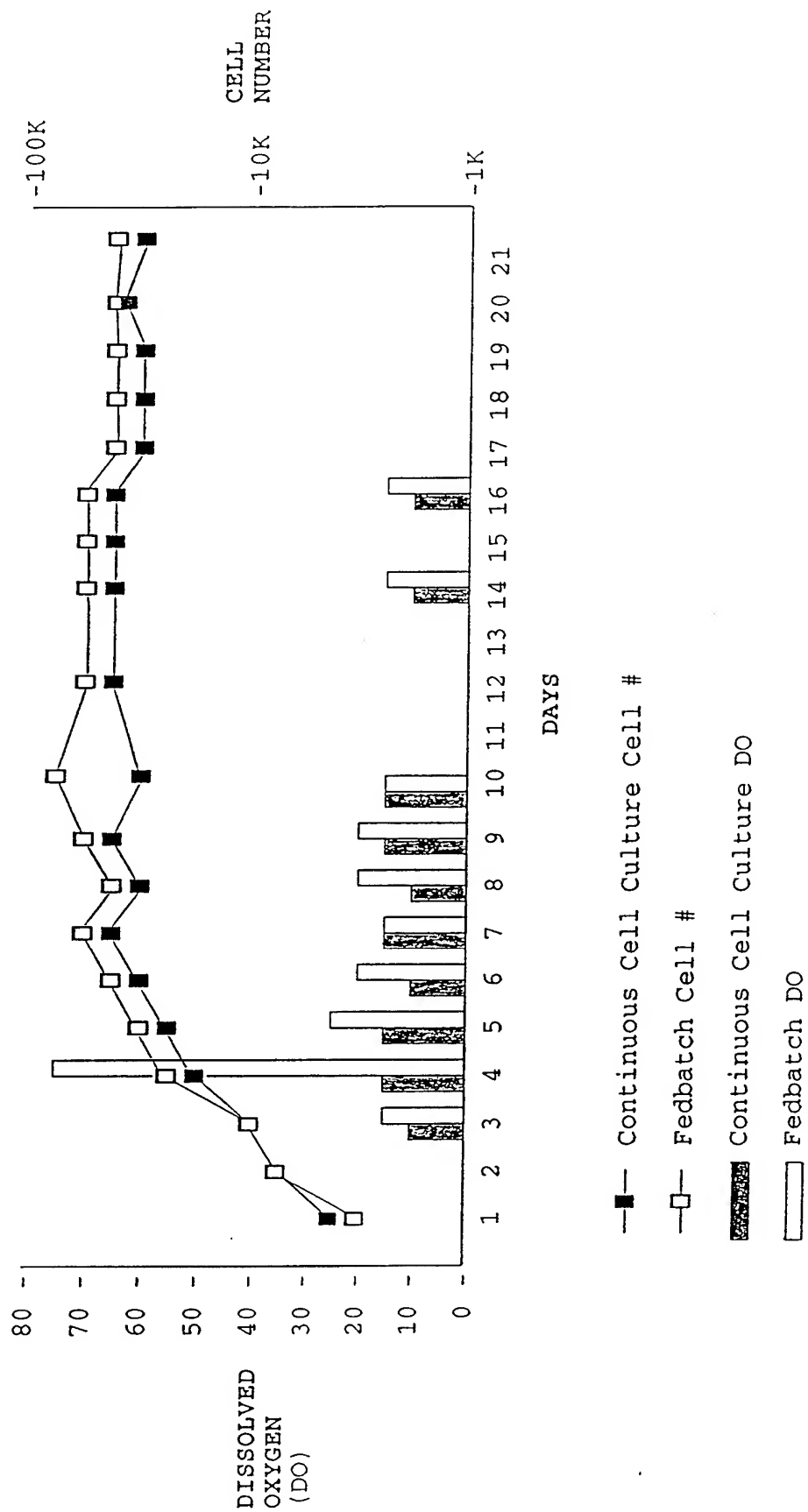


Figure 3



# INTERNATIONAL SEARCH REPORT

International application No.  
PCT/US94/12906

## A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) : C12M 1/02, 1/16; B01D 21/02

US CL : 435/287, 288, 299, 316; 210/143, 194, 513

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 435/287, 288, 299, 316; 210/143, 194, 513

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
Y	US, A, 4,329,433 (SEEBECK et al.) 11 May 1982, see entire document.	1-16
A	US, A, 5,166,072 (KRAULING et al.) 24 November 1992, see entire document.	1-16



Further documents are listed in the continuation of Box C.



See patent family annex.

* Special categories of cited documents:	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be of particular relevance	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"E" earlier document published on or after the international filing date	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"&" document member of the same patent family
"O" document referring to an oral disclosure, use, exhibition or other means	
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search

20 DECEMBER 1994

Date of mailing of the international search report

JAN 23 1995

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